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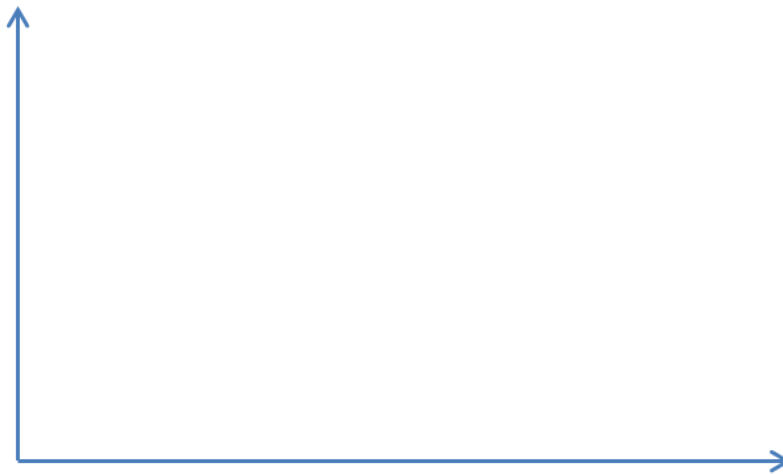
## Biochemical Engineering

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### Exercise Session 7

#### 1) Chemostat Theory

Draw a x-D diagram with consideration of maintenance energy and insert, biomass, volumetric productivity, specific productivity, residual glucose concentration  $s$ ,  $D_{opt}$  and  $D_{crit}$ .



What do you understand under a turbidostat and a pH auxostat?  
What are their differences to a chemostat?

#### 2) Substrate conversion and biomass productivity

A 5 m<sup>3</sup> fermenter is operated continuously with a feed substrate concentration of 20 kg m<sup>-3</sup>. The genetically engineered *E. coli* cultivated in the reactor has the following characteristics:

$$\mu_{\max} = 0.45 \text{ h}^{-1}; K_s = 800 \text{ g m}^{-3}; Y_{X/S} = 0.55 \text{ kg kg}^{-1}$$

- What feed flow rate is required to achieve 90% substrate conversion?
- How does the biomass productivity at 90% substrate conversion compare with the maximum possible?
- What is the biomass concentration in case a) and at the optimal dilution rate?



### 3) Growth inhibition

The specific growth rate for inhibited growth in a chemostat is given by the following equation:

$$\mu = \mu_{\max} S / (K_s + S + I K_s / K_i)$$

Where

$$s_0 = 10 \text{ g L}^{-1}, K_s = 1 \text{ g L}^{-1}; I = 0.05 \text{ g L}^{-1}, Y_{xs} = 0.1 \text{ g g}^{-1}$$

$$x_0 = 0, K_i = 0.01 \text{ g L}^{-1}, \mu_{\max} = 0.5 \text{ h}^{-1}$$

- Determine  $x$  and  $s$  as function of  $D$  when  $I = 0$ .
- With inhibitor added to a chemostat, determine the effluent substrate concentration and  $x$  as function of  $D$ .
- Determine the volumetric cell productivity,  $DX$ , as a function of dilution rate.

#### 4) Wash-out experiment

What is the biomass concentration in a chemostat when one knows the following parameters:

$V = 2.2 \text{ L}$        $F = 200 \text{ mL/h}$   
 $s_0 = 10 \text{ g glucose/L}$      $\mu_{\max} = 0.3 \text{ h}^{-1}$   
 $K_s = 0.2 \text{ g glucose/L}$      $Y_{X/S} = 0.5 \text{ g cells / g glucose}$   
 (consider not metabolized glucose s!)

What is the concentration of the biomass at different times when the dilution rate was changed to  $D = 1.0 \text{ h}^{-1}$ ? Fill in the table below.

Time [h]	Biomass concentration [ $\text{mg L}^{-1}$ ] (3 digits after the comma !)
1	
5	
15	
25	